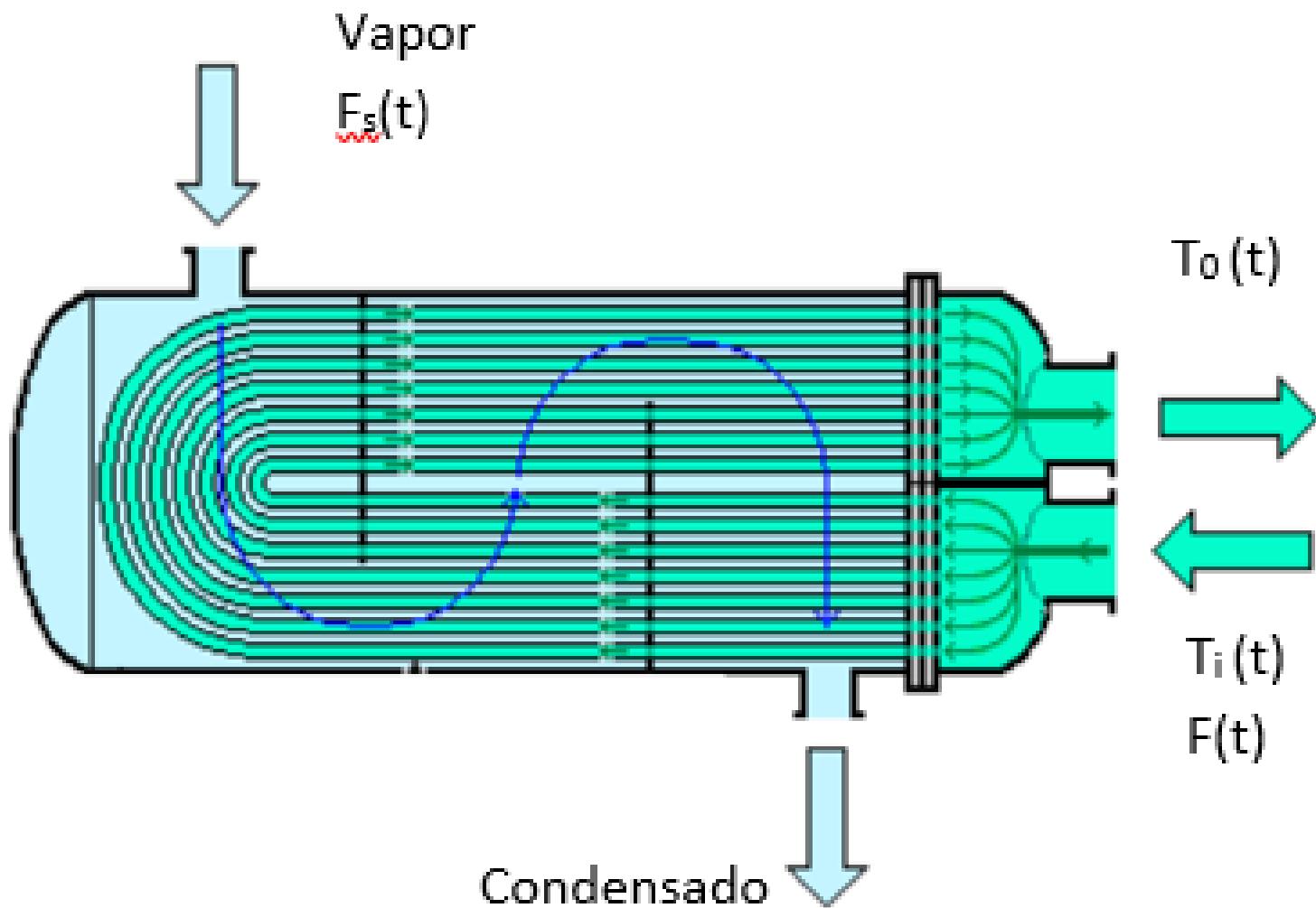
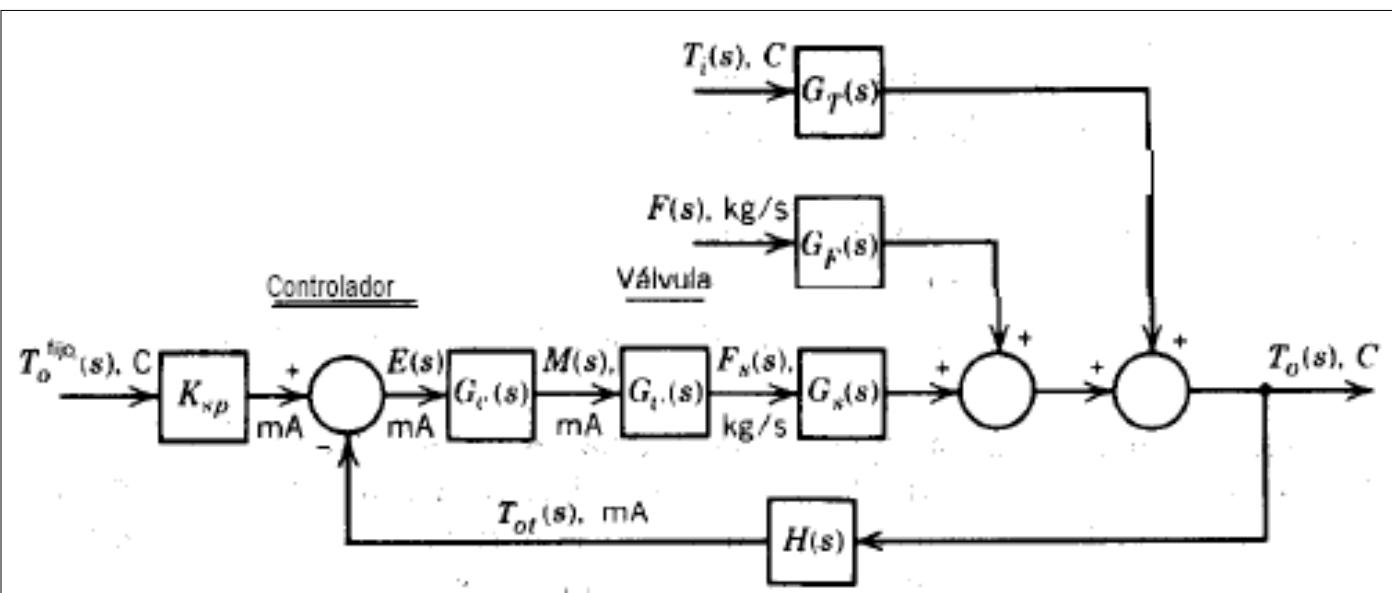
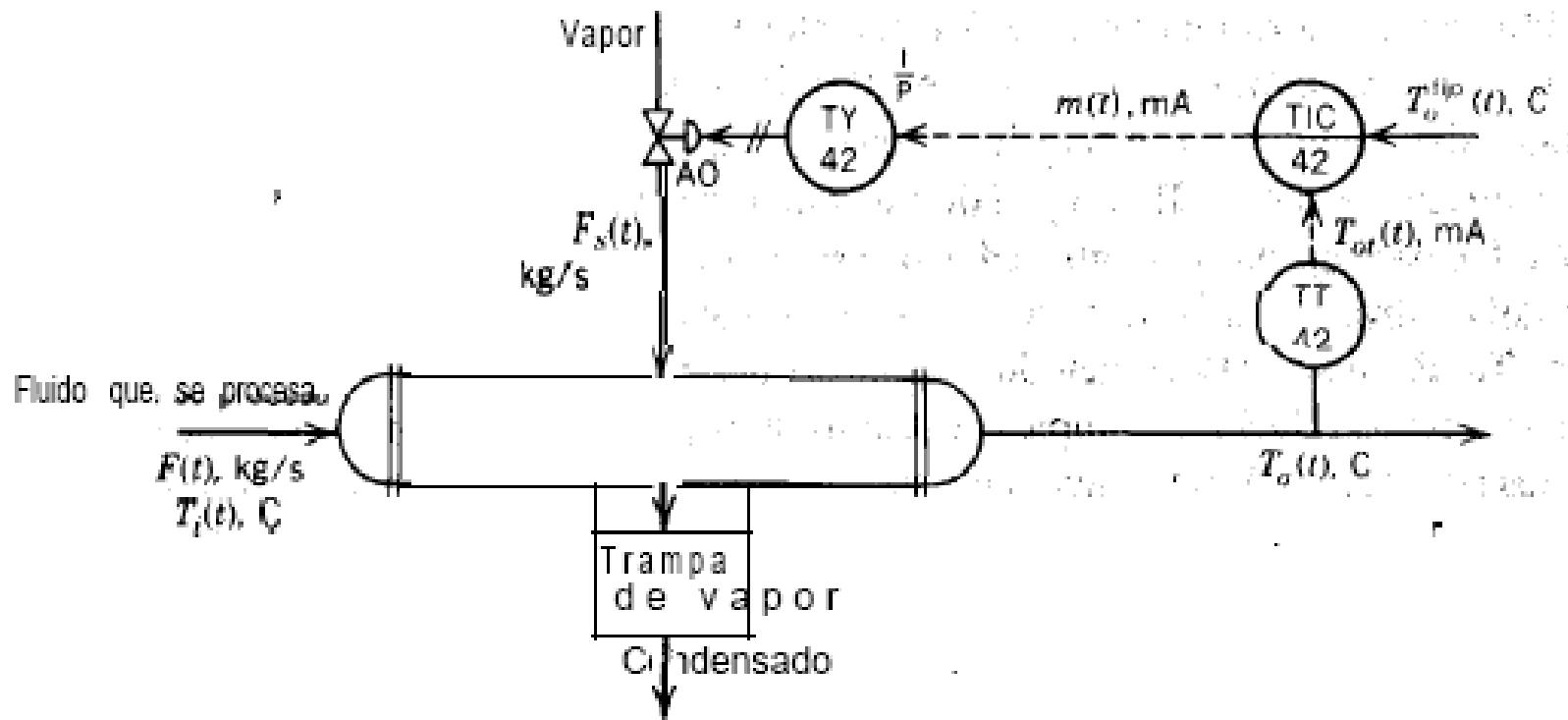
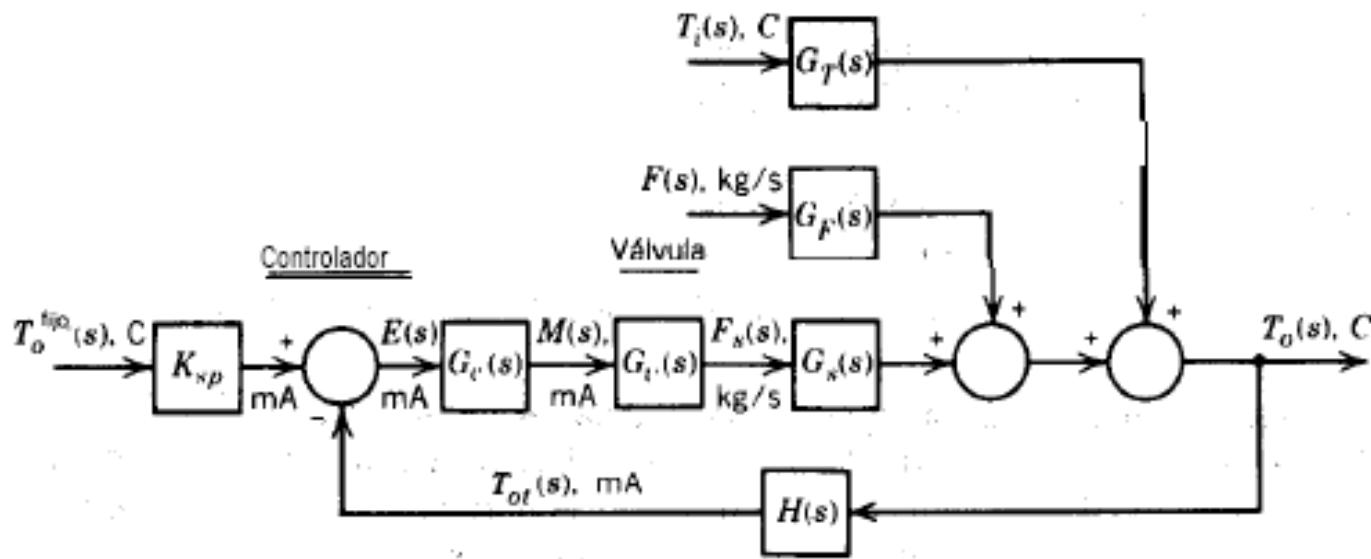


# UNIDAD 2

# ESTABILIDAD







Señal de error:  $E(s) = K_{sp}T_o^{\text{fijo}}(s) - T_{of}(s)$

Variable manipulada:  $M(s) = G_c(s)E(s)$

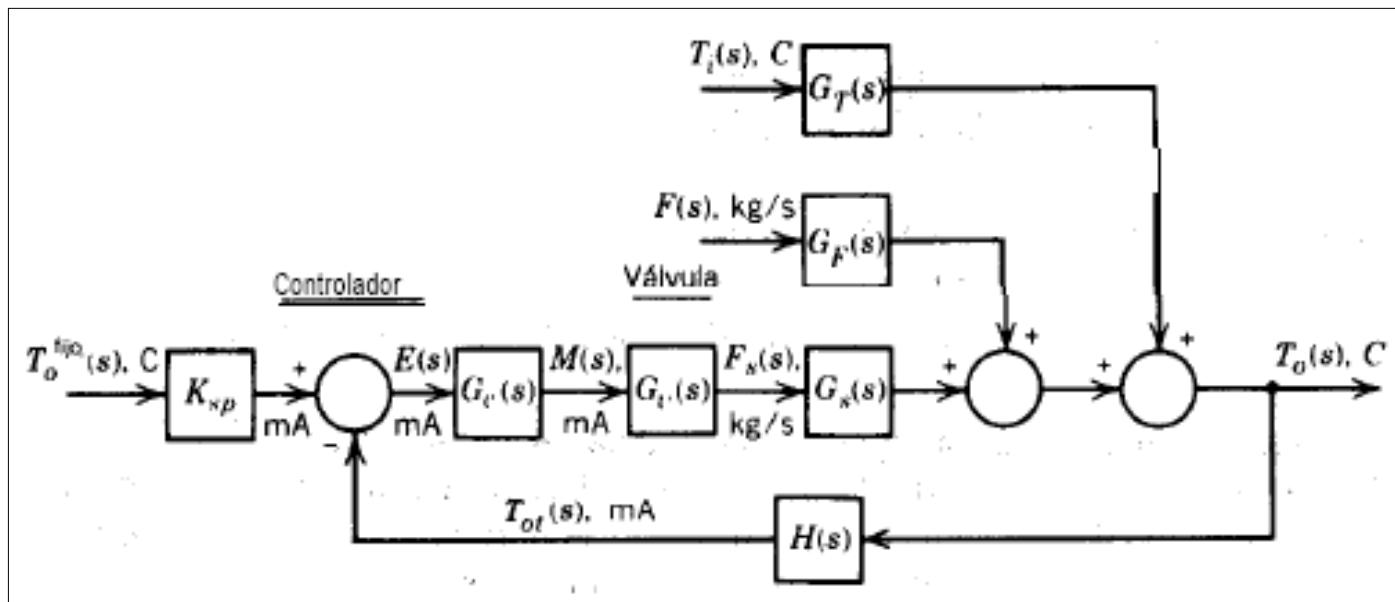
Flujo de vapor:  $F_v(s) = G_v(s)M(s)$

Temperatura de salida:  $T_o(s) = G_s(s)F_v(s) + G_F(s)F(s) + G_T(s)T_i(s)$

Señal del transmisor:  $T_{of}(s) = H(s)T_o(s)$

$$\left. \begin{array}{l} F(s) = 0 \\ T_o^{\text{fijo}}(s) = 0 \end{array} \right\} \longrightarrow T_o(s) = G_s(s)G_v(s)G_c(s)[ - H(s)T_o(s)] + G_T(s)T_i(s)$$

$$\frac{T_o(s)}{T_i(s)} = \frac{G_T(s)}{1 + H(s)G_s(s)G_v(s)G_c(s)}$$



$$\left. \begin{array}{l} T_o^{\text{fijo}}(s) = 0 \\ T_i(s) = 0 \end{array} \right\} \rightarrow \frac{T_o(s)}{F(s)} = \frac{G_F(s)}{1 + H(s) G_i(s) G_v(s) G_c(s)}$$

$$\left. \begin{array}{l} T_i(s) = 0 \\ F(s) = 0 \end{array} \right\} \rightarrow \frac{T_o(s)}{T_o^{\text{set}}(s)} = \frac{G_s(s) G_v(s) G_c(s) K_{sp}}{1 + H(s) G_i(s) G_v(s) G_c(s)}$$

Ecuación característica:

$$1 + H(s) G_i(s) G_v(s) G_c(s) = 0$$

$$T_o(t) = b_1 e^{r_1 t} + b_2 e^{r_2 t} + \dots + b_n e^{r_n t} + (\text{términos de entrada})$$

Respuesta sin forzamiento      Respuesta forzada

$$\left. \begin{array}{l} F(s) = 0 \\ T_o^{\text{fijo}}(s) = 0 \end{array} \right\} \rightarrow \frac{T_o(s)}{T_i(s)} = \frac{G_T(s)}{1 + H(s) G_s(s) G_v(s) G_c(s)}$$

$$\left. \begin{array}{l} T_o^{\text{fijo}}(s) = 0 \\ T_i(s) = 0 \end{array} \right\} \rightarrow \frac{T_o(s)}{F(s)} = \frac{G_F(s)}{1 + H(s) G_s(s) G_v(s) G_c(s)}$$

$$\left. \begin{array}{l} T_i(s) = 0 \\ F(s) = 0 \end{array} \right\} \rightarrow \frac{T_o(s)}{T_o^{\text{set}}(s)} = \frac{G_s(s) G_v(s) G_c(s) K_{sp}}{1 + H(s) G_s(s) G_v(s) G_c(s)}$$

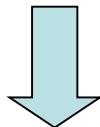
$$a_n s^n + a_{n-1} s^{n-1} + \dots + a_0 = a_n (s - r_1)(s - r_2) \dots (s - r_n) = 0$$

$T_o(s) = \frac{\text{(términos del numerador)}}{a_n(s - r_1)(s - r_2) \dots (s - r_n) \text{(términos de entrada)}}$
---

$T_o(t) = b_1 e^{r_1 t} + b_2 e^{r_2 t} + \dots + b_n e^{r_n t} + \text{(términos de entrada)}$ Respuesta sin forzamiento      Respuesta forzada
---

## Criterio de estabilidad

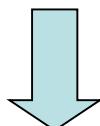
$$c(t) = b_1 e^{r_1 t} + b_2 e^{r_2 t} + \dots + b_n e^{r_n t} + (\text{términos de entrada})$$



Para raíces reales: Si  $r < 0$ , entonces  $e^{rt} \rightarrow 0$  conforme  $t \rightarrow \infty$

Para raíces complejas:  $r = \sigma + i\omega$   $e^{rt} = e^{\sigma t}(\cos \omega t + i \operatorname{sen} \omega t)$

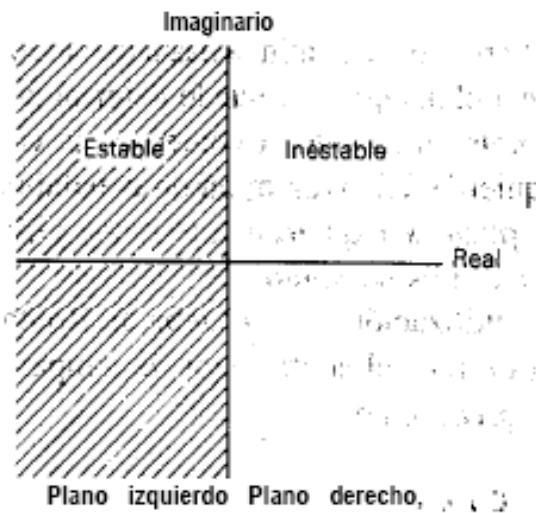
Si  $\sigma < 0$ , entonces  $e^{\sigma t}(\cos \omega t + i \operatorname{sen} \omega t) \rightarrow 0$  conforme  $t \rightarrow \infty$



Para que el circuito de control con retroalimentación sea estable, todas las raíces de su ecuación característica deben ser números reales negativos o números complejos con partes reales negativas.

# Prueba de Routh

Plano s



$$a_n s^n + a_{n-1} s^{n-1} + \dots + a_1 s + a_0 = 0$$

fila 1	$a_n$	$a_{n-2}$	$a_{n-4}$	$\dots$	$a_1$	0
fila 2	$a_{n-1}$	$a_{n-3}$	$a_{n-5}$	$\dots$	$a_0$	0
fila 3	$b_1$	$b_2$	$b_3$	$\dots$	0	0
fila 4	$c_1$	$c_2$	$c_3$	$\dots$	0	0

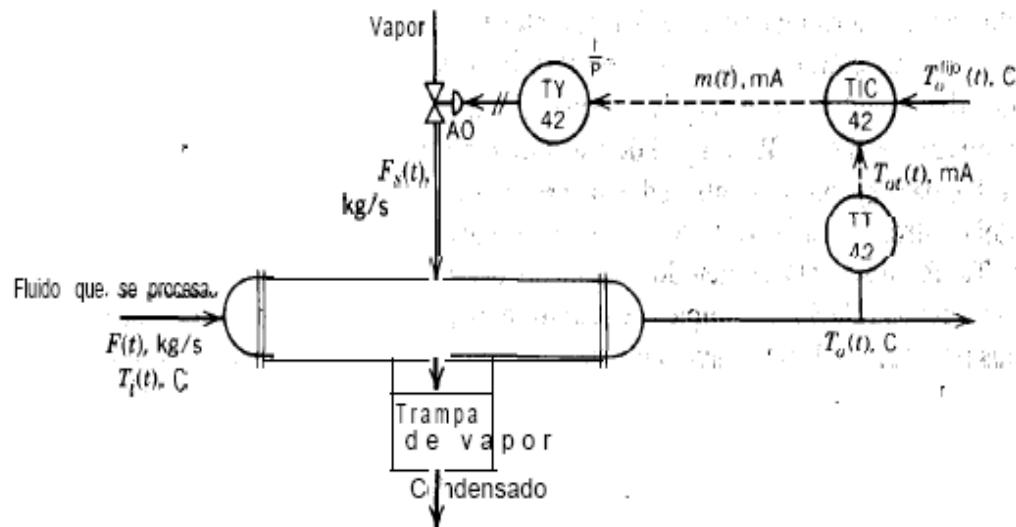
fila n	$d_1$	$d_2$	0	$\dots$	0	0
--------	-------	-------	---	---------	---	---

$$b_1 = \frac{a_{n-1}a_{n-2} - a_n a_{n-3}}{a_{n-1}}, \quad b_2 = \frac{a_{n-1}a_{n-4} - a_n a_{n-5}}{a_{n-1}}$$

$$c_1 = \frac{b_1 a_{n-3} - a_{n-1} b_2}{b_1}, \quad c_2 = \frac{b_1 a_{n-5} - a_{n-1} b_3}{b_1}$$

Intercambiador:

$$G_s(s) = \frac{50}{30s + 1} \text{ C/(kg/s)}$$



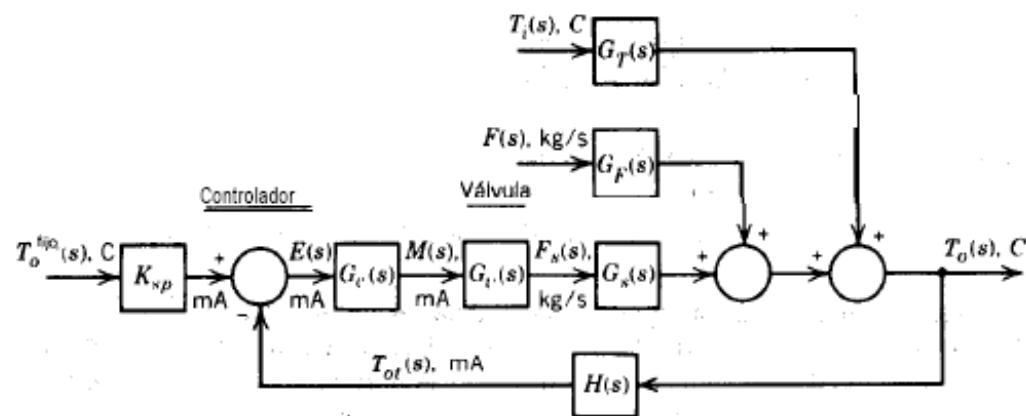
Sensor-transmisor (escala de 50 a 150 °C)

$$H(s) = \frac{1.0}{10s + 1} \%/\text{C}$$

Válvula de control (incluye el conversor I/P):

$$\frac{1.6 (\text{kg/s})}{100\%} = 0.016 (\text{kg/s})/\%$$

$$G_v(s) = \frac{0.016}{3s + 1} (\text{kg/s})/\%$$



Controlador (proporcional)

$$G_c(s) = K_c \%/\%$$

Ecuación característica:  $1 + \left( \frac{50}{30s + 1} \right) \cdot \left( \frac{1}{10s + 1} \right) \cdot \left( \frac{0.016}{3s + 1} \right) \cdot (K_c) = 0$

$$(10s + 1)(30s + 1)(3s + 1) + 0.80Kc = 0 \quad \longrightarrow \quad 900s^3 + 420s^2 + 43s + (1 + 0.80Kc) = 0$$

## Prueba de Routh

$$900.s^3 + 420.s^2 + 43.s + (1 + 0.80.K_c) = 0$$

fila 1	900	43	0
fila 2	420	+ 0.80K <sub>c</sub>	0
fila 3	b <sub>1</sub>	0	0
fila 4	+ 0.80K <sub>c</sub>	0	0

$$b_1 = \frac{(420).(43) - 900.(1 + 0.80.K_c)}{420} = \frac{17160 - 720.K_c}{420}$$

$$b_1 \geq 0 \rightarrow 17160 - 720.K_c \geq 0 \rightarrow K_c \leq 23.8$$

$$1 + 0.80.K_c \geq 0 \rightarrow 0.80.K_c \geq 0 \rightarrow K_c \geq -1.25$$



$K_c \leq 23.8$

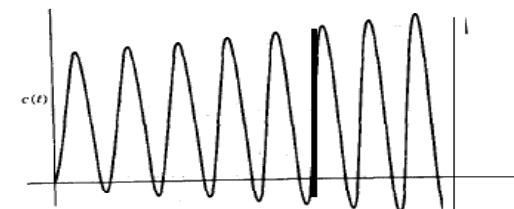
## Método de substitución directa

$$900.s^3 + 420.s^2 + 43.s + (1 + 0.80.Kc) = 0$$

$$s = i\omega$$

$$900.(i\omega)^3 + 420.(i\omega)^2 + 43.(i\omega) + (1 + 0.80.Kc) = 0$$

$$(-420.\omega_u^2 + 1 + 0.80.Kc_u) + i(-900.\omega_u^3 + 43\omega_u) = 0 + i0$$



$$(-420.\omega_u^2 + 1 + 0.80.Kc_u) = 0$$

$$(-900.\omega_u^3 + 43\omega_u) = 0$$



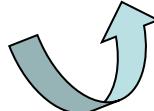
$$\omega_u = 0 \rightarrow Kc_u = -1.25 \frac{\%}{\%}$$

$$\omega_u = 0.22 \text{ rad/seg} \rightarrow Kc_u = 23.8 \frac{\%}{\%}$$

Efecto del tiempo muerto:

$$e^{-t_0 s} \doteq \frac{1 - \gamma_2 t_0 s}{1 + \gamma_2 t_0 s}$$

Aproximación de Padé:



$$\left. \begin{array}{l} G(s) = \frac{K e^{-t_0 s}}{\tau s + 1} \\ G_{r.}(s) = K_c \end{array} \right\} 1 + G \cdot Kc = 0 \rightarrow 1 + \left( \frac{K \cdot e^{-t_0 s}}{\tau \cdot s + 1} \right) \cdot (Kc) = 0$$

$$1 + \left( \frac{K}{\tau \cdot s + 1} \right) \left( \frac{1 - \frac{t_0 s}{2}}{1 + \frac{t_0 s}{2}} \right) \cdot (Kc) = 0$$

$$1 + \frac{K \cdot Kc \left( 1 - \frac{t_0 s}{2} \right)}{(\tau \cdot s + 1) \left( 1 + \frac{t_0 s}{2} \right)} = 0$$



$$1/2 \cdot t_0 \cdot \tau \cdot s^2 + (\tau + 1/2 \cdot t_0 - 1/2 \cdot K \cdot Kc \cdot t_0) s + 1 + K \cdot Kc = 0$$



$$(K \cdot Kc)_u = 1 + 2 \frac{\tau}{t_0}$$

$$\omega_u = \frac{2}{t_0} \sqrt{\frac{t_0}{\tau}} + 1$$

## Auto sintonía de controladores- Kcu y Tu

1. se desconectan las acciones integral y derivativo del controlador, de manera de tener un controlador proporcional. En algunos modelos no es posible desconectar la acción integral, se iguala R al valor máximo.
2. con el controlador cerrando el circuito, se incrementa la acción proporcional constante. Luego se registra el valor de  $K_{cu}$ . Los incrementos deben ser pequeños, en especial al acercarse al valor de oscilación permanente.
3. del registro del tiempo de la variable controlada, se registra y mide el período de oscilación como  $T_u$ , período último, según se muestra en la figura 3.13

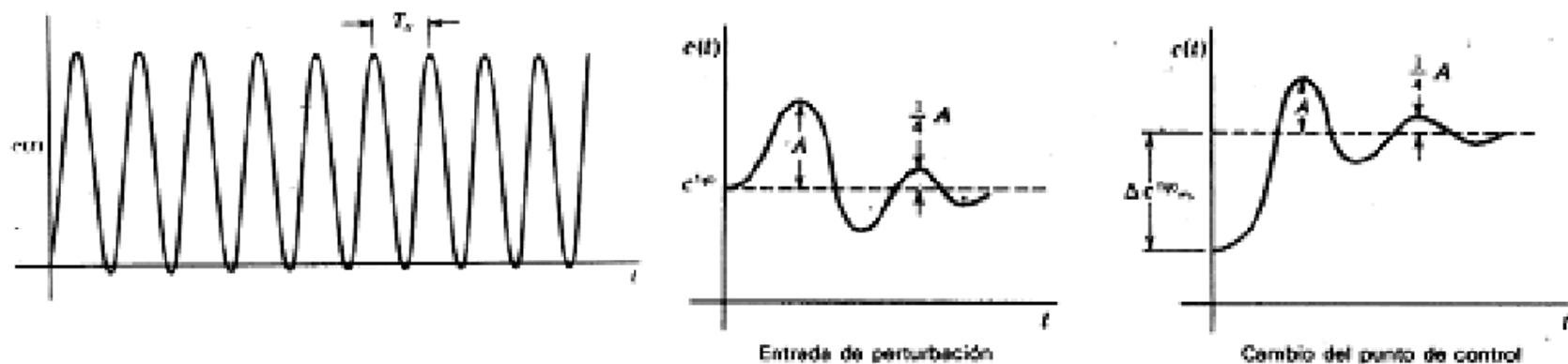


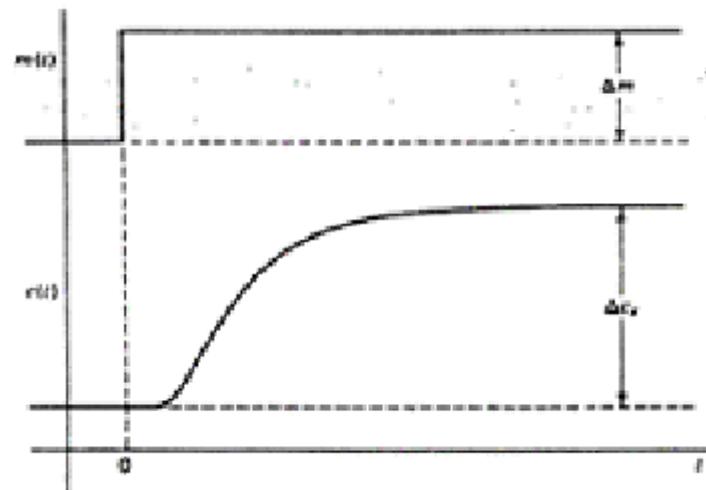
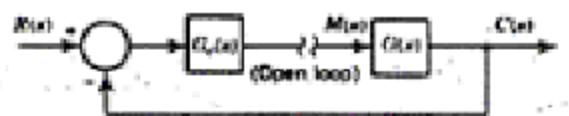
Tabla 6-1 Fórmulas para ajuste de razón de asentamiento de un cuarto.

Tipo de controlador		Ganancia proporcional $K_c$	Tiempo de integración $T_i$	Tiempo de derivación $T_d$
Proporcional	P	$K_{cu}/2$	—	—
Proporcional-integral	PI	$K_{cu}/2.2$	$T_u/1.2$	—
Proporcional-integral-derivativo	PID	$K_{cu}/1.7$	$T_u/2$	$T_u/8$

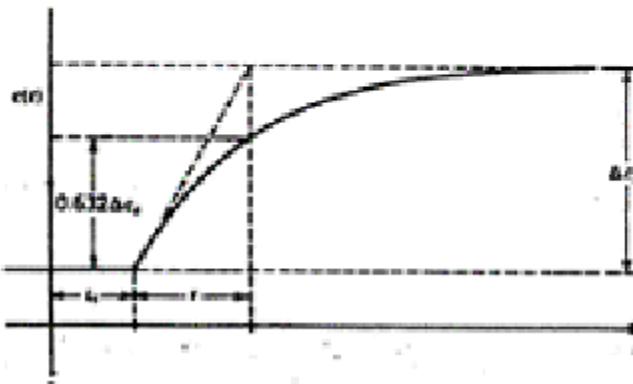
## Caracterización del proceso- Ajuste de controladores

$$C(s) = G(s) \frac{\Delta m}{s}$$

$$C(s) = \frac{K \cdot e^{-t_0 s}}{\tau \cdot s + 1} \frac{\Delta m}{s}$$

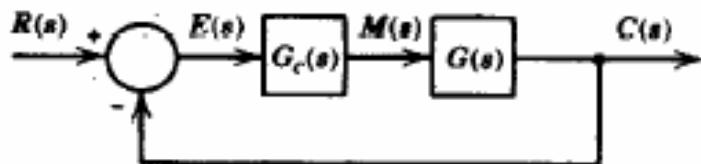


$$K = \frac{\Delta C_s}{\Delta m}$$



Controller Type	Proportional Gain $K_p$	Integral Time $T_i$	Derivative Time $T_d$
Proportional only	P $\frac{1}{K} \left( \frac{t_0}{\tau} \right)^{-1}$	—	—
Proportional-integral	PI $\frac{0.9}{K} \left( \frac{t_0}{\tau} \right)^{-1}$	0.33 $t_0$	—
Proportional-integral-derivative	PID $\frac{1.2}{K} \left( \frac{t_0}{\tau} \right)^{-1}$	2.0 $t_0$	$\frac{1}{2} t_0$

## Método de síntesis directa o ajuste de Dahlin



$$\frac{C(s)}{R(s)} = \frac{G_c(s) G(s)}{1 + G_c(s) G(s)}$$

$$G_c(s) = \frac{1}{G(s)} \frac{C(s) / R(s)}{1 - [C(s) / R(s)]} \quad \longrightarrow \quad G_c(s) = \frac{1}{G(s)} \frac{1}{1 - 1} = \frac{1}{G(s)} \frac{1}{0}$$

$$\frac{C(s)}{R(s)} = \frac{1}{\tau_c s + 1}$$

$$G_c(s) = \frac{1}{G(s)} \frac{1}{\tau_c s}$$

★ Si  $G_p = \frac{1}{\tau s + 1}$  (proceso de primer orden)

$$G_c(s) = \frac{\tau}{K\tau_c} \left(1 + \frac{1}{\tau s}\right) \quad \longrightarrow \quad K_c = \frac{\tau}{K\tau_c} \quad \tau_i = \tau$$

★ Si  $G_p = \frac{K}{(\tau_1 s + 1)(\tau_2 s + 1)}$  (proceso de segundo orden)  $\longrightarrow G_c(s) = \frac{\tau_1}{K\tau_c} \left(1 + \frac{1}{\tau_1 s}\right) (\tau_2 s + 1)$

$$\text{Modelo del proceso : } G(s) = \frac{K e^{-\zeta s}}{\tau s + 1}$$

Controlador proporcional (P):  $G_c(s) = K_c$

Integral del error	ICE	IAE	IAET
$K_c = \frac{a}{K} \left( \frac{t_0}{\tau} \right)^{b_1}$	$a = 1.411$	0.902	0.490
	$b = -0.917$	-0.985	-1.064

Controlador proporcional-integral (PI)

$$G_c(s) = K_c \left( 1 + \frac{1}{\tau_i s} \right)$$

Integral de error	ICE	IAE	IAET
$K_c = \frac{a_1}{K} \left( \frac{t_0}{\tau} \right)^{b_1}$	$a_1 = 1.305$	0.984	0.859
	$b_1 = -0.959$	-0.986	-0.977
$\tau_i = \frac{\tau}{a_2} \left( \frac{t_0}{\tau} \right)^{b_2}$	$a_2 = 0.492$	0.608	0.674
	$b_2 = 0.739$	0.707	0.680

Controlador proporcional-integral-derivativo (PID):

$$G_c(s) = K_c \left( 1 + \frac{1}{\tau_i s} + \tau_o s \right)$$

Integral de error	ICE	IAE	IAET
$K_c = \frac{a_1}{K} \left( \frac{t_0}{\tau} \right)^{b_1}$	$a_1 = 1.495$	1.435	1.357
	$b_1 = -0.945$	-0.921	-0.947
$\tau_i = \frac{\tau}{a_2} \left( \frac{t_0}{\tau} \right)^{b_2}$	$a_2 = 1.101$	0.878	0.842
	$b_2 = 0.771$	0.749	0.738
$\tau_o = \theta_3 \tau \left( \frac{t_0}{\tau} \right)^{b_3}$	$a_3 = 0.560$	0.482	0.381
	$b_3 = 1.006$	1.137	0.995

Ziegler - Nichols	Ziegler-Nichols	IAE	Dahlin
$K_c = \frac{1,2}{K} \left( \frac{\tau}{\tau_d} \right)$	$K_c = \frac{K_{cn}}{1,7}$	$K_c = \frac{a_1}{K} \left( \frac{\tau_d}{\tau} \right)^{b_1}$  <div style="border: 1px solid orange; padding: 5px;"><math>a_1 = 1,435</math> <math>b_1 = -0,921</math></div>	$K_c = \frac{\tau}{K(\tau_d + \tau_c)}$ <div style="border: 1px solid orange; padding: 5px;"><math>\tau_c = \frac{1}{5} \tau_d</math></div>
$R = 2\tau_d$	$R = \frac{\tau_u}{2}$	$R = \frac{\tau}{a_2} \left( \frac{\tau_d}{\tau} \right)^{b_2}$ <div style="border: 1px solid orange; padding: 5px;"><math>a_2 = 0,878</math> <math>b_2 = 0,749</math></div>	$R = \tau$
$D = \frac{\tau_d}{2}$	$D = \frac{\tau_u}{8}$	$D = a_3 \tau \left( \frac{\tau_d}{\tau} \right)^{b_3}$ <div style="border: 1px solid orange; padding: 5px;"><math>a_3 = 0,482</math> <math>b_3 = 1,137</math></div>	$D = \frac{\tau_d}{2}$

## Lugar de raíces

$$G(s) = \frac{Gc \cdot Gp}{1 + Gc \cdot Gp}$$

Función de transferencia  
de lazo cerrado

Si:

$$Gc(s) = Kc$$

$$Gp(s) = \frac{1}{s(s+1)}$$

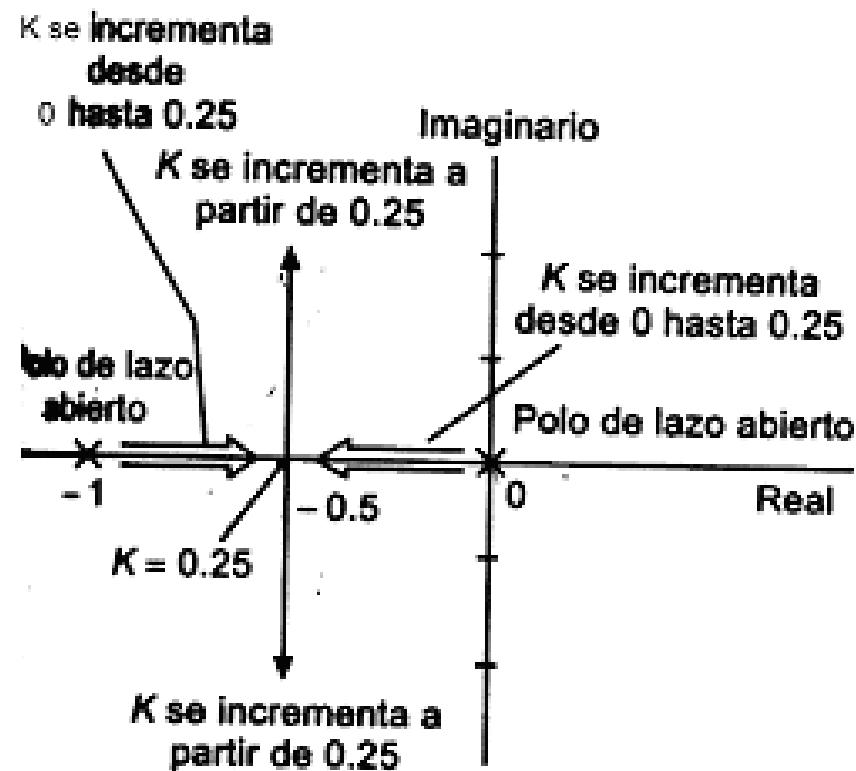
$$G(s) = \frac{Kc / [s(s+1)]}{1 + Kc / [s(s+1)]}$$

$$G(s) = \frac{Kc}{s^2 + s + Kc}$$

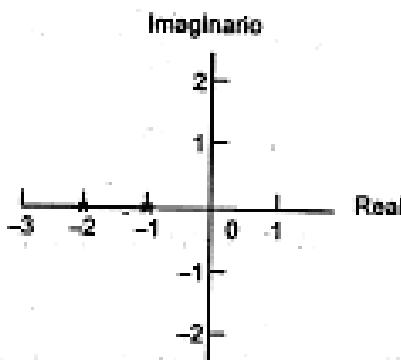
Las raíces del polinomio del denominador de la función de transferencia son:

$$p = \frac{-1 \pm \sqrt{1 - 4Kc}}{2}$$

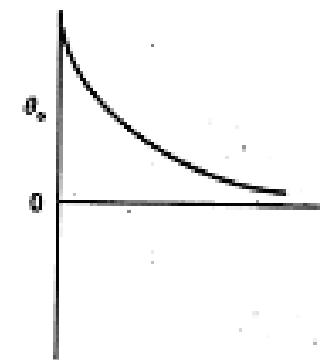
$$p = -\frac{1}{2} \pm \frac{1}{2} \sqrt{1 - 4Kc}$$



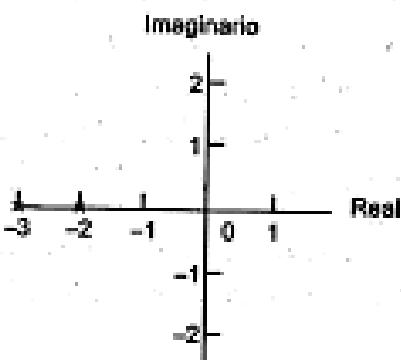
Raíz= -1



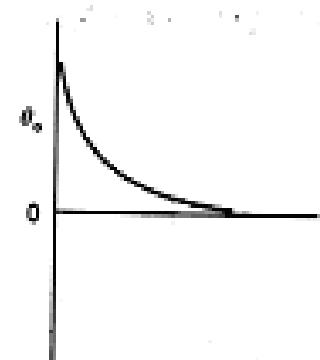
a)



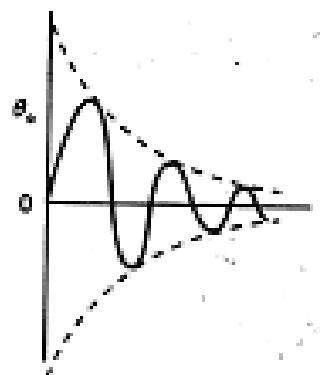
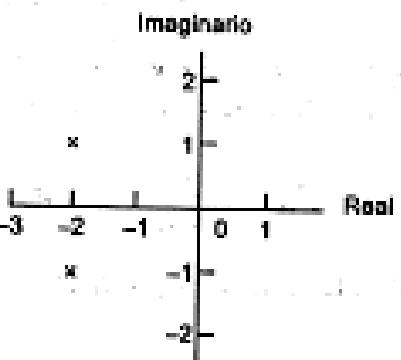
Raíz= -2



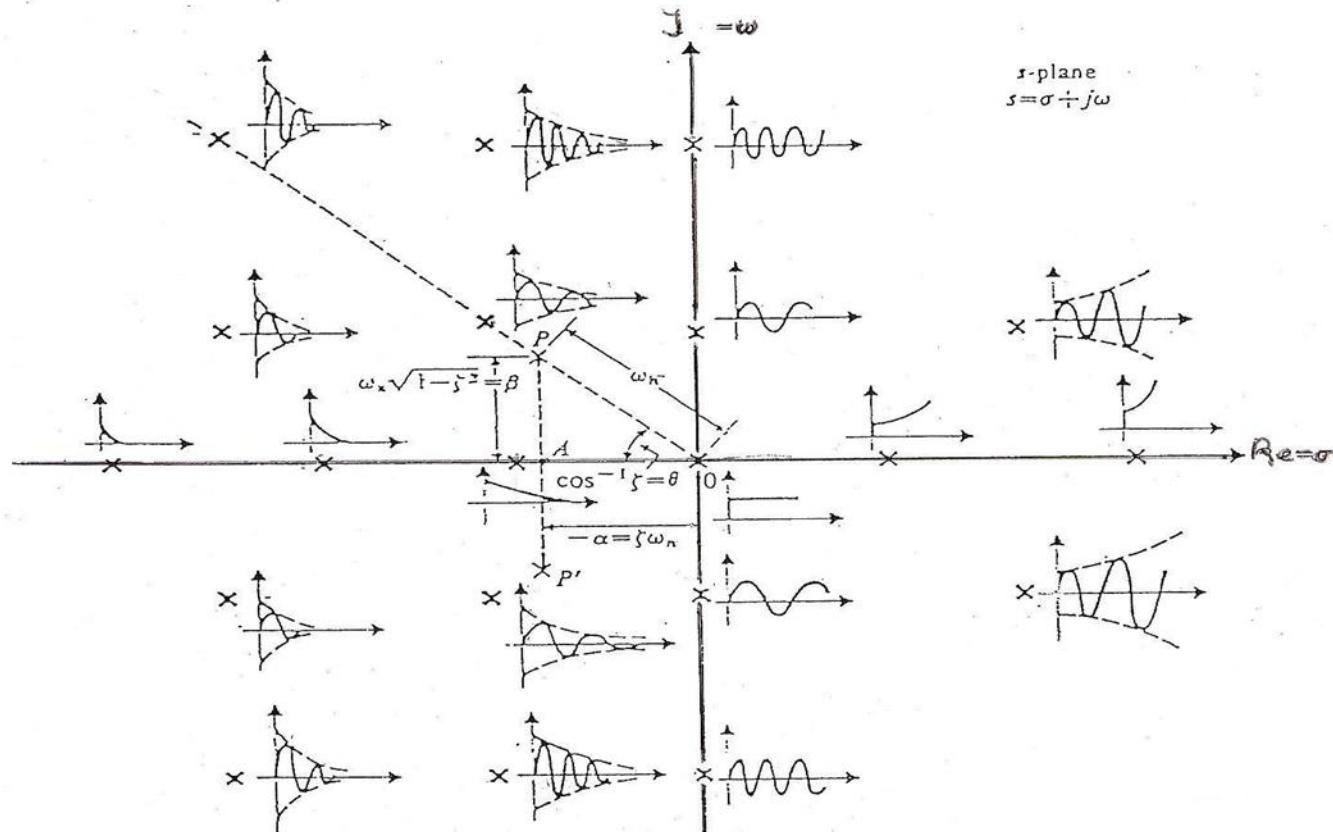
b)



Raíces=  $-2+1j$   
 $-2-1j$



Scalar input-output linear systems and feedback control



$$G(s) = \frac{K \prod (s - z_j)}{\prod (s - p_i)} \quad \text{Significance of root location in the } s\text{-plane.}$$

$$\frac{\prod [(s + \alpha_j)^2 + \beta_j^2]}{\prod [(s + \alpha_i)^2 + \beta_i^2]} = \frac{K \prod (1 + 2\zeta_j s + (z_j s)^2)}{\prod (1 + 2\zeta_i s + (z_i s)^2)}$$